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AN EXPLOSION PREVENTION VENTING SYSTEM

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AN EXPLOSION PROTECTION VENTING SYSTEM

The present application is related to U.S. Application Serial Number _____, filed _____ of Robert C. Knyrim and Timothy F. Simmons, and entitled, "Flame Front Diverter Element", Atty. Docket No. 5 85220/CEB.

FIELD OF THE INVENTION

The invention relates generally to the field of explosion protection systems. More specifically, the invention relates to a flame front diverter element when used in an explosion protection venting system having a plurality of vessels 10 diverts a deflagration in a different direction than the normal flow path thereby virtually eliminating any impending disastrous effects to surrounding structure.

BACKGROUND OF THE INVENTION

According to maximum achievable control technology (MACT) and European regulations, emerging emission standards will affect most 15 manufacturing areas containing operational vents to atmosphere. A cost-effective strategy for treating hazardous flammable solvent emissions is to manifold operational vessel vents together to one emission control device. However, in the unexpected event of a flammable solvent ignition, there is a possibility of fire or deflagration propagation, which could potentially destroy any or all the devices 20 connected in the vent system. Therefore, fire and explosion protection schemes must be in place to minimize potential consequences of a fire or explosion. Prior art includes an explosion diverter or backflash interrupter to prevent flames from propagating from one piece of equipment to another through the interconnecting piping.

25 The basic principle of operation of a typical device as described above is that a deflagration is vented in a different flow direction than the normal flow path. Due to the inertia of the fast flow caused by the deflagration, the flow will tend to maintain its direction upward rather than making the hard degree turn as when the vessel emission flow velocity is low during normal conditions. When 30 the high-speed deflagration flame continues upward, it pushes open either a hinged cover or bursts a rupture disc located at the top of the diverter, allowing the flame to be released to the atmosphere. The limitations placed on the existing

device are that it can only be used in processes with a combustible dust with very low concentrations. The operating pressure is limited to 0.1 barg (1.5 psig) due to the pressure setting of the relief device required for approval.

Another device to prevent propagation during a deflagration is the 5 explosion isolation valve. There are high-speed sensors installed on both sides of the isolation valve to detect a high rate of pressure rise in the pipeline and then close the valve before the deflagration can pass through. This is an expensive scheme with no guarantee that the valve will close before the deflagration or flame passes through.

10 Therefore, a need persists in the art for an explosion protection venting system having a flame front diverter element that diverts deflagration along an alternate path and away from the normal flow path that avoids a disastrous impact to nearby structures.

SUMMARY OF THE INVENTION

15 The present invention is directed to overcoming one or more of the problems set forth above. Briefly summarized, according to one aspect of the present invention, an explosion protection venting system has a plurality of connected vessels, such as reactors. Each one of the plurality of vessels has a vent in fluid communications with a common connection line between the plurality of 20 vessels. A flame front diverter is connected to each one of the plurality of vessels. The flame front diverter has an elongated channel that has opposing first and second end portions and a rupturable disc in fluid communications with the elongated channel mounted to each of the opposing first and second end portions. First and second vapor flow channels are disposed in the elongated channel. Either 25 of the first and second vapor flow channels is connected to the common connection line to receive process vapor and to form a primary flow path for process vapor propagation between the elongated channel and the other of the first and second vapor flow channels to a downstream process. In this manner, effluent produced by excessive pressure caused by combustion of the process vapor is 30 diverted away from the primary flow path and through one of the rupturable disc that ruptures outwardly from the elongated channel. Further, the other of the rupturable disc ruptures inwardly of the elongated channel causing an

instantaneous stream of outside air to flow inwardly of the elongated channel between each of the rupturable discs thereby interrupting the combustion process.

The present invention has the following advantages over prior art developments, including: it is a passive system with no moving parts; it will work 5 up to about 5 psig operating pressure; it will operate at a vapor throughput rate up to about 350 fit/min; and, it will mitigate any deflagration independent of the starting point in any pipeline connected to the venting system.

BRIEF DESCRIPTION OF THE DRAWINGS

The above and other objects, features, and advantages of the 10 present invention will become more apparent when taken in conjunction with the following description and drawings wherein identical reference numerals have been used, where possible, to designate identical features that are common to the figures, and wherein:

Fig. 1 is a side view of the flame diverter element of the invention; 15 Fig. 2 is an end view of the rupturable disc used in accordance with the invention;

Fig. 3 is a perspective view of the flame front diverter partially exploded to show the rupturable discs displaced during a deflagration; and,

Fig. 4 is a schematic of an explosion protection venting system of 20 the invention.

DETAILED DESCRIPTION OF THE INVENTION

Turning now to the drawings, and in particular to FIGS. 1 and 3, the flame front diverter element 10 of the invention is illustrated. According to FIG. 1, flame front diverter element 10 has an elongated channel 12 having 25 opposing first and second end portions 14, 16. A rupturable disc 18, 20 is arranged in fluid communications with the elongated channel 12. Either one of rupturable disc 18, 20 is mounted to one of the opposing first and second end portions 14, 16 of elongated channel 12.

According to FIG. 1, a first vapor flow channel 22 disposed in an 30 end portion of elongated channel 12 has an inlet end 24 and outlet end 26. Similarly, a second vapor flow channel 28 disposed in an opposing end portion of elongated channel 12 has an inlet end 30 and an outlet end 32. Preferably first and

second vapor flow channels 22, 28 are welded to elongated channel although other attachment means, such as bolting, may work with similar success. It is important to the invention that the inlet end 30 has a predetermined spacing (d) from the nearest rupturable disc 20. Each rupturable discs 18, 20 is sandwiched between a 5 pair of opposing flanges 27, 29, respectively, fixedly mounted to the elongated channel 12.

Referring again to FIG. 1, flanges 27, 29 each has a diameter of about 4 inches and a force rating of 150 lbs to withstand the deflagration pressure. It is our experience that the inlet end 30 of vapor flow channel 28 is preferably 10 spaced apart 5/8 inch to 1½ inches from rupturable disc 20 at setup. Outside the lower spacing limit, i.e., 5/8 inch, the flame diverter element 10 has been observed to plug-up. Beyond the upper spacing limit, i.e., 1½ inch, the opposing rupturable disc 18 may not rupture. Similarly, it is important that the outlet end 26 of vapor flow channel 22 has a predetermined spacing (d') from nearest rupturable disc 18 15 at the other end of the elongated channel 12. According to our testing outlet end 26 is preferably spaced apart 5/8 inch to 1½ inch from rupturable disc 18 at setup. Outside the lower spacing limit, i.e., 5/8 inch, the flame diverter element 10 has been observed to plug-up. Beyond the upper spacing limit, i.e., 1½ inch, the opposing rupturable disc 20 may not rupture. Moreover, either of the first and 20 second vapor flow channels 22, 28 is configured to receive process vapor from a flammable process and to form a primary flow path 34 for process vapor propagation between the elongated channel 12 and the other of the first and second vapor flow channels 22, 28 to a downstream process.

It is preferred that elongated channel 12 has a wall thickness of at 25 least 0.237 inches and the vapor flow channels 22, 28 has a wall thickness of at least 0.139 inches to withstand peak deflagration pressure.

Further, rupturable discs 18, 20 are each bi-directional relative to the elongated channel 12 so that a deflagration can be vented in either direction relative to the interconnected vessel or reactor (see fig 4). Also, rupturable discs 30 18, 20 are capable of rupturing at a pressure of not more than about 5 psig. The dual bi-directional rupturable discs 18, 20 are to account for the possibility that a deflagration can start on either side of the flame front diverter element 10.

Referring to FIG. 3, once the deflagration starts, one rupturable disc 18, 20 will burst outwards from the pressure ahead of the flame front diverter element 10 at 0.34barg (5psig) potentially producing fragments 21. The high deflagration flow rate creates an aspiration effect on the opposite rupturable disc 18, 20 causing it to burst inwards forming potentially jagged edges 23 or fragmented pieces 21 of the disc inside elongated channel 12. This allows a rush of ambient air into the elongated channel 12 to obstruct the continual flow of hot gases downstream of the flame front diverter 10.

Referring to FIG. 4, according to another embodiment of the invention, flame front diverter element 10 is specifically designed for installation in an explosion protection system 100 from a plurality of vessels 102 (for instance reactors) manifold together to a final emission control element 104. In this embodiment, flame front diverter element 10 (described above) is connected to each of the vent lines 106 associated with each vessel 102 and final emission control element 104. If a vessel 102 has an internal deflagration, other vessels 102 connected in the vent line 106 could become involved with the initial deflagration. Skilled artisans will appreciate that flame front diverter element 10 is designed to prevent a deflagration from propagating from one vessel 102 to another vessel 102 or to the final emission control element 104. The operating conditions of the explosion protection system 100 can be higher than prior art design flow rates, any flammable solvent concentration, and up to operating pressure of 0.34barg (5psig).

Referring again to FIG. 4, flame front diverter element 10 is designed to cause a minimal pressure drop under normal venting conditions when process vapors need to pass through the explosion protection system 100 and to other equipment connected to the manifold system. In the event of a deflagration, the flame front diverter 10 directs the high-speed pressure wave towards a bi-directional rupturable disc 18, 20 causing the rupturable disc 18, 20 to open thus creating an aspiration effect on the opposite bi-directional rupturable disc 18, 20. Fresh air immediately is caused to enter the elongated channel 12 to interrupt the continuous hot gas flow, thus stopping the downstream deflagration propagation. As shown in FIG. 4, flame diverter element 10 can be installed in the manifold

system between each vessel 102 /process equipment and upstream of an emission control element 104 in the atmospheric vent line 106 containing flammable vapors.

The invention has been described with reference to a preferred 5 embodiment. However, it will be appreciated that a person of ordinary skill in the art can effect variations and modifications without departing from the scope of the invention.

PARTS LIST

- 10 flame front diverter element
- 12 elongated channel
- 14 end portion
- 16 end portion
- 18 rupturable disc
- 20 rupturable disc
- 21 fragments/fragmented pieces
- 22 first vapor flow channel
- 23 jagged edges
- 24 inlet end
- 26 outlet end
- 27 flange
- 28 second vapor flow channel
- 29 flange
- 30 inlet end
- 32 outlet end
- 34 flow path
- 100 explosion protection system
- 102 vessel
- 104 final emission control element
- 106 vent line